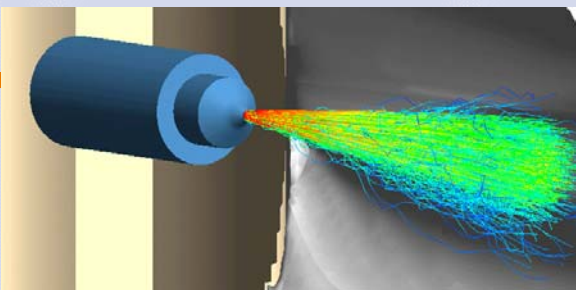




# Mercury Control Evaluation of Halogen Injection into a Texas Lignite-Fired Boiler



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# Addition of Halogen-Containing Species to Flue Gas

- **Oxidation of mercury in flue gas**
  - Hg speciation related to flue gas HCl content
  - Higher Hg oxidation may increase Hg removal across flue gas path
- **For low-chloride coals, inject halogen species into boiler**
  - Increases Hg oxidation in flue gas
  - Potential for enhanced fly ash reactivity
  - Increase in Hg removal across wet scrubber
  - EPRI testing since 2002 shows promising results
    - Lignite and PRB coals

# EPRI Chemical Addition Test Objectives

- Increase mercury oxidation in flue gas derived from Texas lignite
- Enhance mercury removal across wet scrubbers
- Parametric Tests
  - $\text{CaCl}_2$  – vary injection rates
  - $\text{CaBr}_2$  – limited 3-hour test at one rate

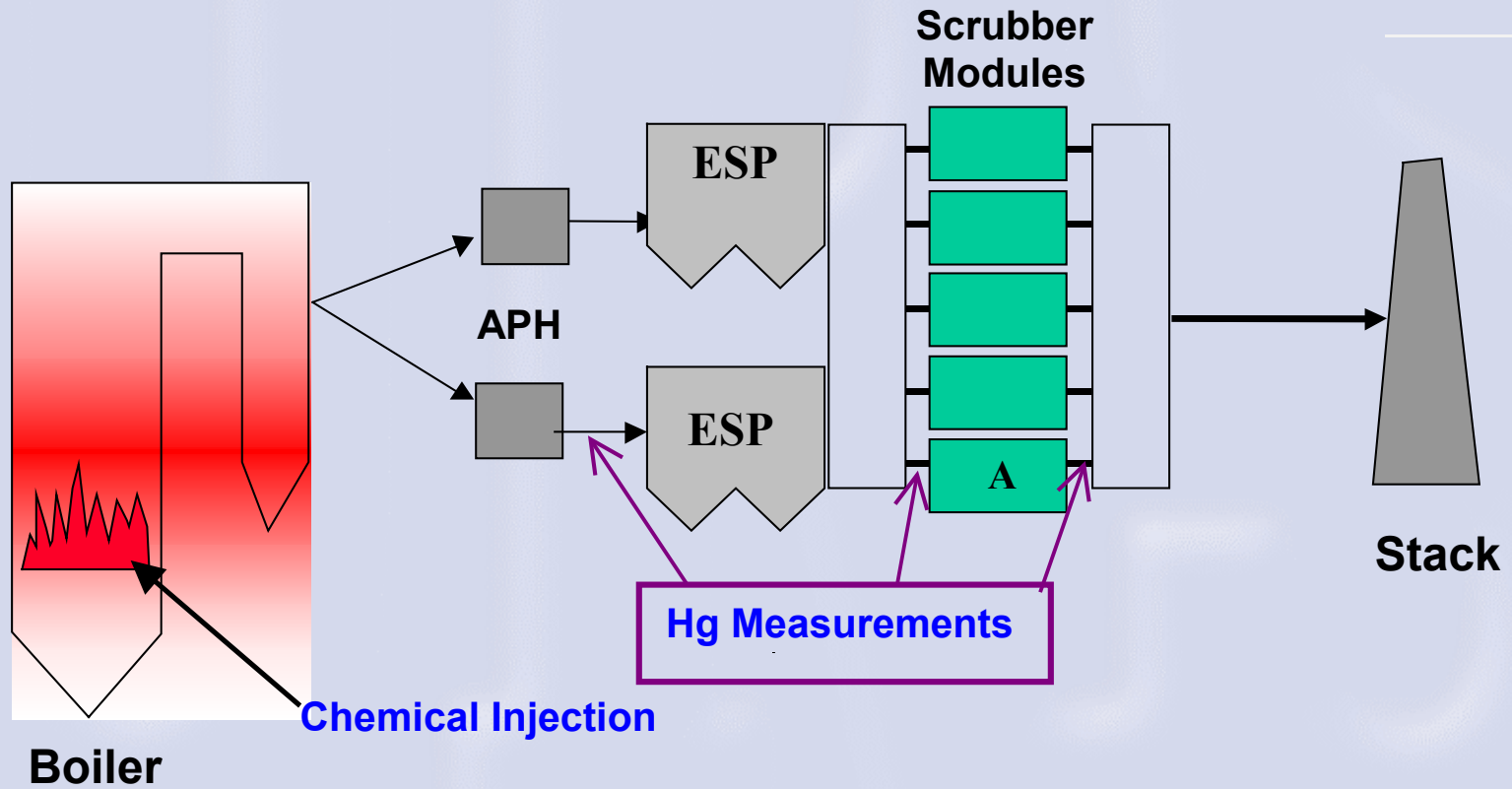
# Host Site - Texas Genco's Limestone Electric Generating Station

- Unit 1- 890 MW
- Inject into half of split furnace



# Chemical Injection

## Limestone Station Unit 1





# Fuel Parameters During Testing at Limestone

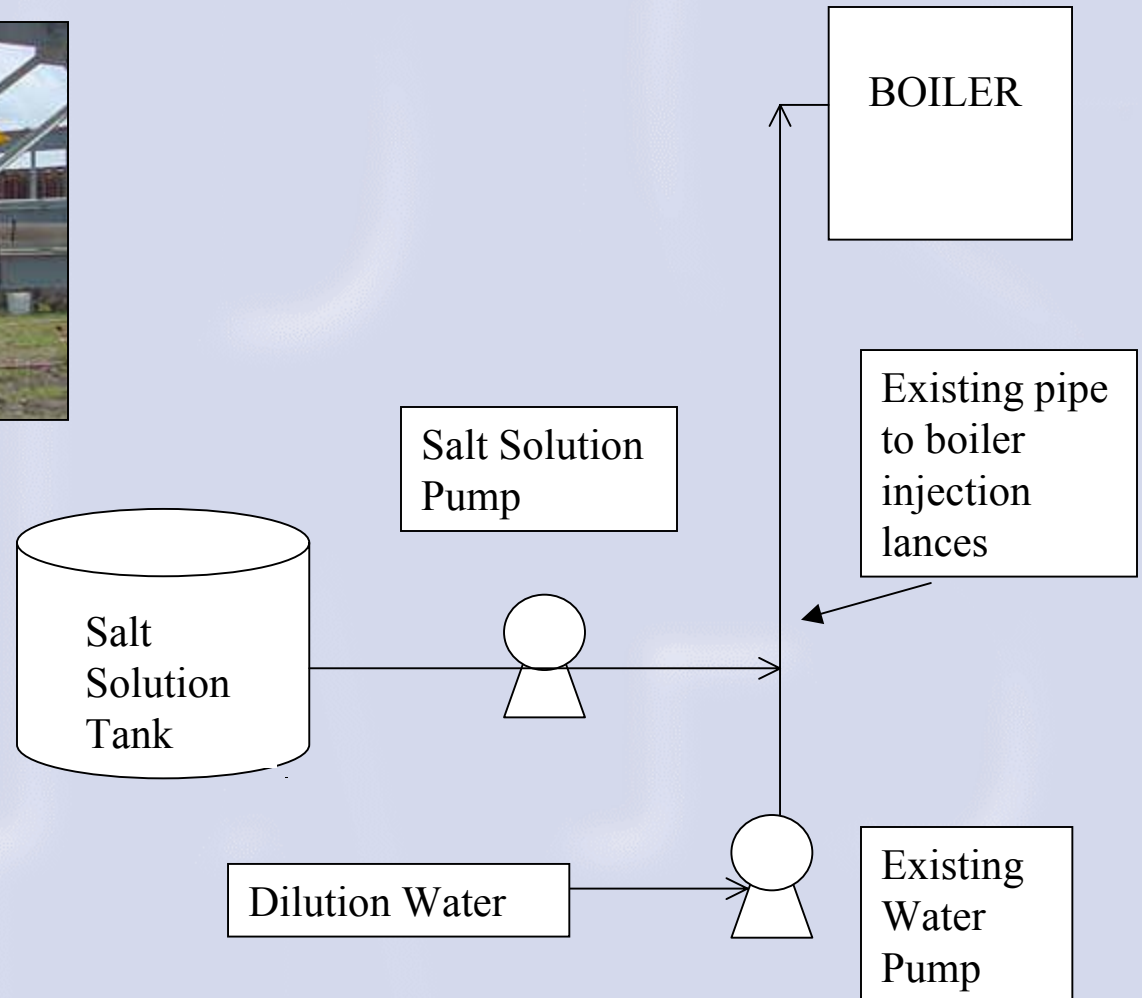
Fuel Type	Texas Lignite	PRB
Heating Value (as received)	5500-6900 Btu/lb	7900-8300 Btu/lb
Ash	15-27%	4-8%
Sulfur	0.9-1%	0.3-0.5%
Water	29-32 %	30%
Mercury	0.15-0.22 ppm	0.06-0.10 ppm
Chlorine	50-100 ppm	25-60 ppm

# Baseline Mercury Measurements

- Hg at ESP Inlet = 23-33  $\mu\text{g}/\text{Nm}^3$  at 3%  $\text{O}_2$
- 45% Oxidation at ESP Inlet
- Baseline HCl = 3 ppm
- Hg vapor removal by fly ash < 5%
- System Hg vapor removal = 50 to 65%



# Schematic of Injection Equipment

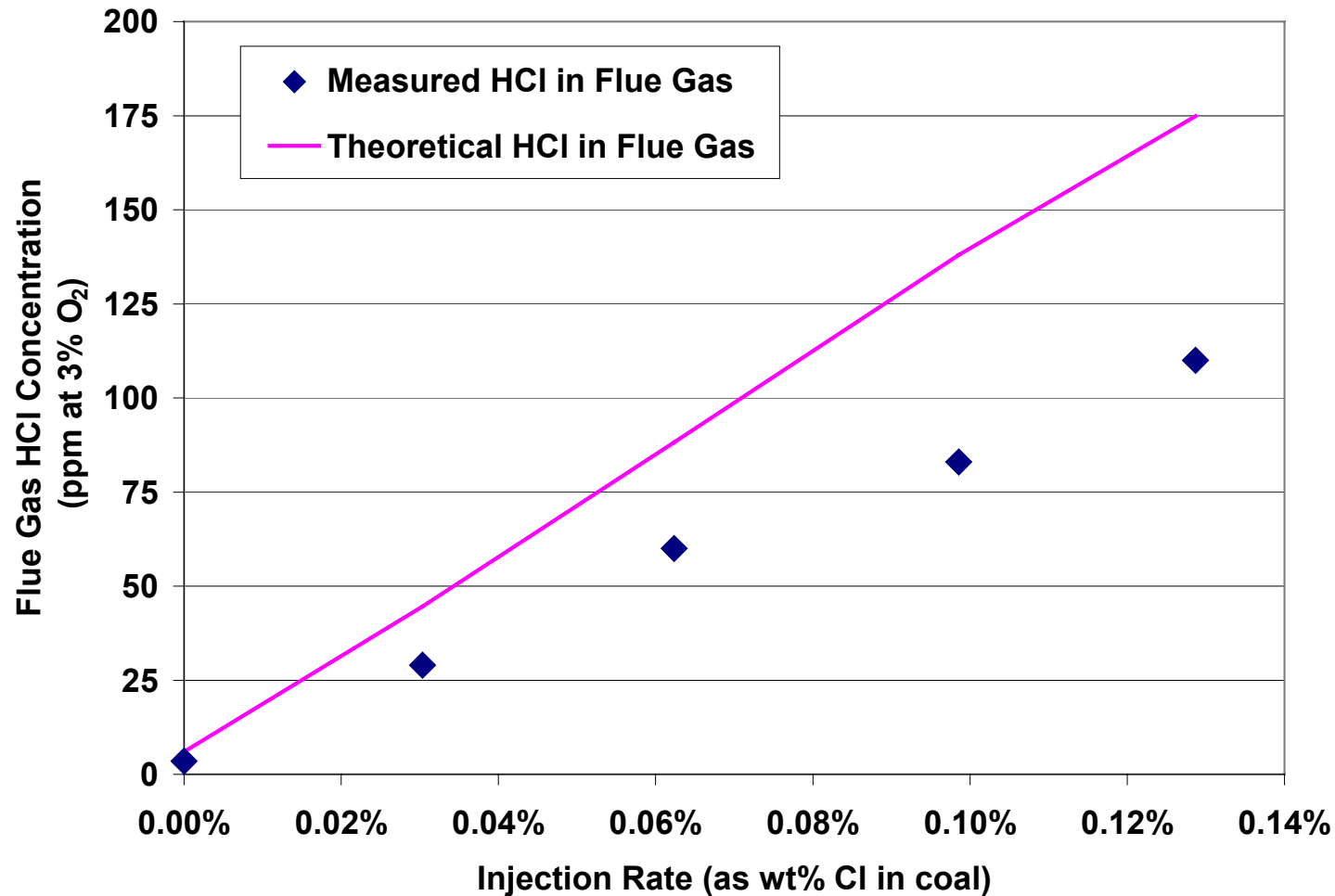




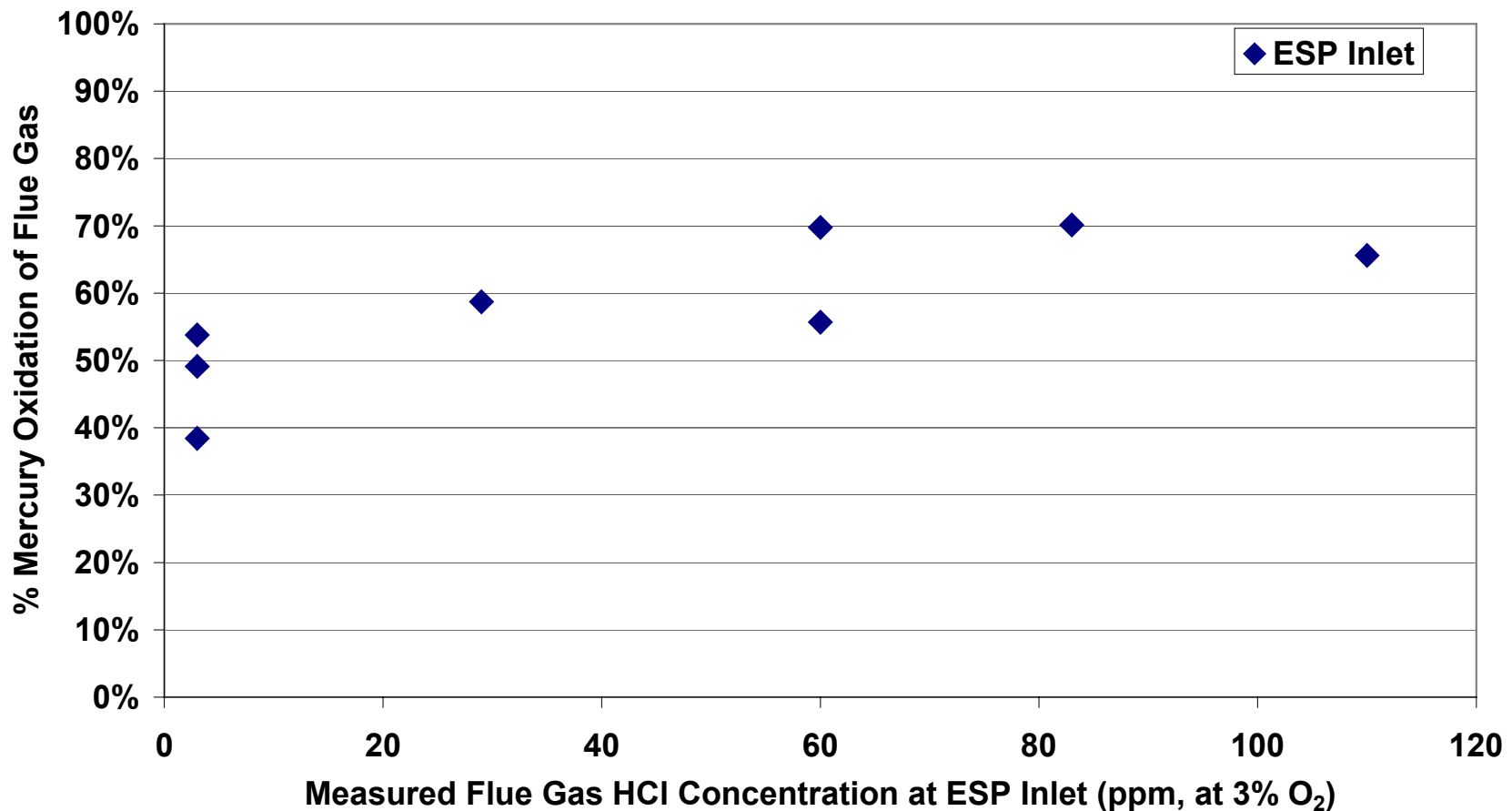
# Chemical Addition to Unit 1 Boiler Limestone Station

Salt	Weight % Chloride/ Bromide (% relative to coal)	Liquid Salt Feed Rate (gpm)	Theoretical Gas Conc. (ppm HCl or ppm HBr)
<b>CaCl<sub>2</sub></b> <b>(25 wt%)</b>	<b>0.03</b>	<b>1.9</b>	<b>40</b>
	<b>0.06</b>	<b>4.0</b>	<b>80</b>
	<b>0.10</b>	<b>6.4</b>	<b>120</b>
	<b>0.13</b>	<b>8.2</b>	<b>155</b>
<b>CaBr<sub>2</sub></b> <b>(52 wt%)</b>	<b>0.09</b>	<b>1.6</b>	<b>50</b>

# Effect of $\text{CaCl}_2$ Addition Limestone Station



# CaCl<sub>2</sub> Effect on Hg Oxidation at ESP Inlet

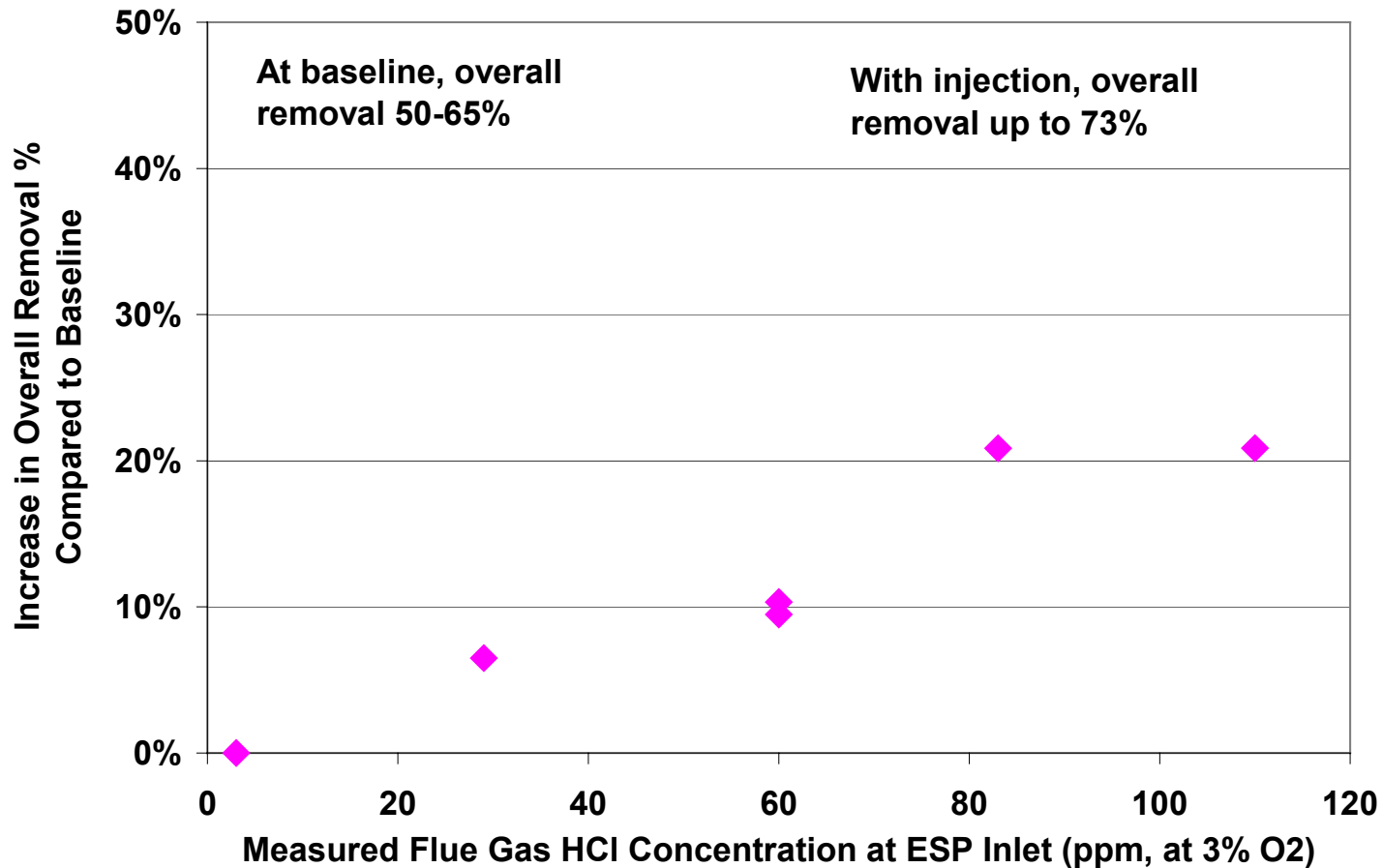


# % Removal of Hg across System

- Compares the ESP inlet Hg to the FGD outlet Hg.
- Includes both native removal and effect of  $\text{CaCl}_2$  injection.
- Calculated as:

$$\text{Removal across ESP/FGD} = 100 * \left( 1 - \frac{Hg_{FGD \text{ Out, Inj}}^{\text{Total}}}{Hg_{ESP \text{ In, Inj}}^{\text{Total}}} \right)$$

# Increase in System Hg Removal Percentage - $\text{CaCl}_2$ Tests





# Effect of $\text{CaBr}_2$ Tests

- Limited, three-hour test of calcium bromide
- Injected 0.09 wt% as Br in coal
  - 48 ppm HBr in flue gas
- Results:
  - 81% overall removal across ESP/FGD  
(observed 73% removal with 60 ppm Cl)

# Summary

- **Oxidation of mercury increased with each salt tested**
  - **Oxidation at ESP Inlet increased from 45% to 70%**
- **Scrubber removal enhanced**
  - **With  $\text{CaCl}_2$  injection, achieved as high as 73% system Hg removal**
  - **With  $\text{CaBr}_2$  injection, achieved 81% system removal**

# Further Testing Needed

- Evaluate long-term operation
- Characterization of potential balance-of-plant impacts of chemical injection
  - Boiler corrosion
  - Air heater plugging
  - FGD performance
  - FGD materials of construction

# Plan Forward

- Additional Tests Planned at Limestone for 2005-2006
  - Process optimization tests
  - Balance of plant determinations
- Project team is soliciting participation from other Power Generators

# Plan Forward

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