

Gulf Drilling Guides



Gas Well Deliquification

Solutions to Gas Well Liquid Loading Problems

James Lea Henry V. Nickens Michael Wells



GAS WELL DELIQUIFICATION

GAS WELL DELIQUIFICATION

JAMES LEA
HENRY NICKENS
MICHAEL WELLS



Gulf Professional Publishing is an imprint of Elsevier.

Copyright © 2003, Elsevier (USA). All rights reserved.

No part of this publication may be reproduced, stored in a retrieval system, or transmitted in any form or by any means, electronic, mechanical, photocopying, recording, or otherwise, without the prior written permission of the publisher.

© Recognizing the importance of preserving what has been written, Elsevier prints its books on acid-free paper whenever possible.

International Standard Book Number 0-7506-7724-4

British Library Cataloguing-in-Publication Data

A catalogue record for this book is available from the British Library.

The publisher offers special discounts on bulk orders of this book. For information, please contact:

Manager of Special Sales Elsevier 200 Wheeler Road Burlington, MA 01803 Tel: 781-313-4700 Fax: 781-313-4882

For information on all Gulf Professional Publishing publications available, contact our World Wide Web home page at: http://www.gulfpp.com

10 9 8 7 6 5 4 3 2 1

Printed in the United States of America

CONTENTS

D C	
Preface	X111

2

1 Introduction 1

1.1 Introduction 1

1.2	Multiphase Flow In A Gas Well 2
1.3	What Is Liquid Loading? 4
1.4	Problems Caused By Liquid Loading 5
1.5	Deliquefying Techniques 6
1.6	Source of Liquids In A Producing Gas Well 8
	1.6.1 Water Coning 8
	1.6.2 Aquifer Water 8
	1.6.3 Water Produced from Another Zone 8
	1.6.4 Free Formation Water 9
	1.6.5 Water of Condensation 9
	1.6.6 Hydrocarbon Condensates 9
	References 11
	gnizing Symptoms of Liquid Loading in Gas Wells 13
2.1	Introduction 13
	Presence of Orifice Pressure Spikes 14
	Decline Curve Analysis 14
	Drop in Tubing Pressure with Rise in Casing Pressure 15
	Pressure Survey Showing Tubing Liquid Level 18
	Well Performance Monitoring 21
2.7	Annulus Heading 21
	2.7.1 Heading Cycle without Packer 21
	2.7.2 Heading Cycle Controls 23
2.8	Liquid Production Ceases 25
	*
2.9	Summary 25 References 26

vi Contents

3	Critica	al Velocity 27
	3.1	Introduction 27
	3.2	Critical Flow Concepts 27
		3.2.1 Turner Droplet Model 27
		3.2.2 Critical Rate 30
		3.2.3 Critical Tubing Diameter 31
		3.2.4 Critical Rate for Low Pressure Wells—Coleman Model 31
		3.2.5 Critical Flow Nomographs 34
	3.3	Critical Velocity at Depth 38
	3.4	Critical Velocity in Horizontal Well Flow 40
		References 41
4	System	ns Nodal Analysis 43
	4.1	Introduction 43
	4.2	Tubing Performance Curve 45
	4.3	Reservoir Inflow Performance Relationship (IPR) 46
		4.3.1 Gas Well Backpressure Equation 47
		4.3.2 Future IPR Curve with Backpressure Equation 49
	4.4	Intersections of the Tubing Curve and the
		Deliverability Curve 49
	4.5	Tubing Stability and Flowpoint 52
	4.6	Tight Gas Reservoirs 53
	4.7	Nodal Example—Tubing Size 54
	4.8	Nodal Example—Surface Pressure Effects: Use Compression to
		Lower Surface Pressure 55
	4.9	Summary Nodal Example of Developing IPR from Test Date
		with Tubing Performance 56
	4.10	Summary 60
		References 60
5		Tubing 61
	5.1	Introduction 61
	5.2	Advantages and Disadvantages of Smaller Tubing 61
	5.3	Concepts Required to Size Smaller Tubing 62
		5.3.1 Critical Rate at Surface Conditions 65
		5.3.2 Critical Rate at Bottomhole Conditions 65
		5.3.3 Summary of Tubing Design Concepts 66
	5.4	Sizing Tubing without IPR Information 67
	5.5	Field Example No. 1—Results of Tubing Changeout 69
	5.6	Field Example No. 2—Results of Tubing Changeout 69
	5.7	Pre- and Post-Evaluation 71

5.8 Where to Set the Tubing 72

Contents

	5.9	Hanging Off Smaller Tubing from the Current Tubing	74
	5.10	Summary 76	
		References 76	
6	Comp	ression 79	
	6.1	Introduction 79	
	6.2	Nodal Example 80	
	6.3	Compression with a Tight Gas Reservoir 81	
	6.4	Compression with Plunger Lift Systems 82	
	6.5	Compression with Beam Pumping Systems 84	
	6.6	Compression with Electric Submersible Systems 85	
	6.7	Types of Compressors 85	
		6.7.1 Rotary Lobe Compressor 86	
		6.7.2 Re-Injected Rotary Lobe Compressor 86	
		6.7.3 Rotary Vane Compressor 86	
		6.7.4 Liquid Ring Compressor 87	
		6.7.5 Liquid Injected Rotary Screw Compressor 87	
		6.7.6 Reciprocating Compressor 88	
		6.7.7 Sliding Vane Compressor 89	
	6.8	Gas Jet Compressors or Eductors 90	
	6.9	Summary 92	
		References 93	
7	Plunge	er Lift 95	
	7.1	Introduction 95	
	7.2	Plungers 97	
	7.3	Plunger Cycle 99	
	7.4	Plunger Lift Feasibility 100	
		7.4.1 GLR Rule of Thumb 101	
		7.4.2 Feasibility Charts 102	
		7.4.3 Maximum Liquid Production with Plunger Lift	105
		7.4.4 Plunger Lift with Packer Installed 106	
		7.4.5 Plunger Lift Nodal Analysis 107	
	7.5	Plunger System Line-Out Procedure 108	
		7.5.1 Considerations Before Kickoff 109	
		7.5.2 Kickoff 111	
		7.5.3 Cycle Adjustment 112	
		7.5.4 Stabilization Period 113	
		7.5.5 Optimization 113	
		7.5.6 Monitoring 115	
	7.6	Problem Analysis 116	
		7.6.1 Motor Valve 118	
		7.6.2 Controller 121	

viii Contents

		7.6.3 Arrival Transducer 123
		7.6.4 Wellhead Leaks 124
		7.6.5 Catcher Not Functioning 124
		7.6.6 Pressure Sensor Not Functioning 125
		7.6.7 Control Gas to Stay on Measurement Chart 126
		7.6.8 Plunger Operations 126
		7.6.9 Head Gas Bleeding Off Too Slowly 133
		7.6.10 Head Gas Creating Surface Equipment Problems 134
		7.6.11 Low Production 135
		7.6.12 Well Loads up Frequently 135
	7.7	
		New Plunger Concept 136
	7.8	Operation with Weak Wells 138
		7.8.1 Casing Plunger for Weak Wells 138
		7.8.2 Plunger with Side String: Low Pressure Well
	7 0	Production 142
	7.9	Plunger Summary 144
		References 144
8	Lico of	f Foam to Deliquefy Gas Wells 147
o	8.1	Introduction 147
	8.2	Liquid Removal Process 148
	0.2	
	0.2	8.2.1 Surface De-Foaming 150 Foam Selection 150
	8.3	
	8.4	Foam Basics 153 8.4.1 Foam Generation 153
		8.4.2 Foam Stability 153
		8.4.3 Surfactant Types 155
	0.5	8.4.4 Foaming with Brine/Condensate Mixtures 158
	8.5	Operating Considerations 163
		8.5.1 Surfactant Selection 163
		8.5.2 Bureau of Mines Testing Procedures 163
		8.5.3 Unloading Techniques and Equipment 166
		8.5.4 Determining Surface Surfactant Concentration 169
		8.5.5 Instrumentation 173
	0.6	8.5.6 Chemical Treatment Problems 173
	8.6	Summary 174
		References 175
9	Hydra	nulic Pumps 177
,	9.1	Introduction 177
	9.1	Advantages and Disadvantages 182
	9.3	The 1 1/4-Inch Jet Pump 185
	9.3 9.4	System Comparative Costs 188
	フ. ✝	System Comparative Costs 100

Contents ix

	9.5 9.6	Hydraulic Pump Case Histories 188 Summary 189
		References 189
10	Use of	Beam Pumps to Deliquefy Gas Wells 191
		Introduction 191
		Basics of Beam Pump Operation 193
	10.3	
		10.3.1 Design Rate with Pump-Off Control 196
		10.3.2 Use of Surface Indications for Pump-Off Control 197
	10.4	Gas Separation to Keep Gas Out of the Pump 199
		10.4.1 Set Pump Below the Perforations 200
		10.4.2 "Poor-Boy" or Limited-Entry Gas Separator 201
		10.4.3 Collar-Sized Separator 202
	10.5	Handling Gas through the Pump 203
		10.5.1 Compression Ratio 204
		10.5.2 Variable Slippage Pump to Prevent Gas-Lock 206
		10.5.3 Pump Compression with Dual Chambers 206
		10.5.4 Pumps that Open the Traveling Valve
		Mechanically 206
		10.5.5 Pumps to Take the Fluid Load Off the Traveling
		Valve 206
	10.6	Inject Liquids Below a Packer 207
	10.7	Other Problems Indicated by the Shape of the Pump
		Card 209
	10.8	Summary 213
		References 214
11	Gas L	ift 215
	11.1	Introduction 215
	11.2	Continuous Gas Lift 217
		11.2.1 Basic Principles of Continuous Gas Lift 217
	11.3	Intermittent Gas Lift 217
		Gas Lift System Components 218
		Continuous Gas Lift Design Objectives 220
	11.6	· · · · · · · · · · · · · · · · · · ·
		11.6.1 Orifice Valves 222
		11.6.2 IPO Valves 222
		11.6.3 PPO Valves 223
	11.7	Gas Lift Completions 224
		11.7.1 Conventional Gas Lift Design 224
		11.7.2 Chamber Lift Installations 227
		11.7.3 Horizontal Well Installations 229

X Contents

12

13

14

	11.7.4 Coiled Tubing Gas Lift Completions 231 11.7.5 Gas Pump Concept 234 11.7.6 Gas Circulation 235 Gas Lift without Gas Lift Valves 235 Summary 236 References 237
Electi	ric Submersible Pumps 239
12.1	Introduction 239
12.2	ESP System 240
12.3	ESP System 240 What Is A "Gassy" Well? 243
12.4	Completions and Separators 245
	Injection of Produced Water 248
12.6	Summary 248
	References 250
Drog	ressive Cavity Pumps 251
	Introduction 251
	PCP System Selection 253
13.2	13.2.1 Rotor 253
	13.2.2 Stator 254
	13.2.3 Surface Drive 257
13.3	
15.5	13.3.1 Important Factors for Sizing the System 257
	13.3.1 Important Factors for Sizing the System 25713.3.2 Steps to Size the PCP 259
13.4	Ancillary Equipment 263
10	13.4.1 Flow Detection Devices 264
	13.4.2 Rod Guides 265
	13.4.3 Gas Separators 265
	13.4.4 Tubing Anchor/Catcher 266
13.5	
13.5 13.6	Summary 268
	References 268
Othor	Mothods to Attach Liquid Loading Droblems 271
	: Methods to Attach Liquid-Loading Problems 271 Introduction 271
14.1	
17.4	
	14.2.1 Thermal Lift 273 14.2.2 Thermal Liner 276
	14.2.2 Thermal Chief 276 14.2.3 Thermal Coatings/Liners 277
	14.2.4 With Packer Installed, Draw a Vacuum on
	the Annulus 278
14.3	Cycling 278
17.3	Cycling 270

Contents

14.5	Tubing Flow Control 280
14.6	Tubing Collar Inserts for Producing Below
	Critical Velocity 281
14.7	Summary 282
	References 282
	A: Development of Critical Velocity Equations 283
A.1	Introduction 283
	A.1.1 Physical Model 283
A.2	Equation Simplification 286
A.3	Turner Equations 287
A.4	Coleman Equations 287
	References 288
Annondiza	D. Davidanment of Dlungar Lift Equations 200
	B: Development of Plunger Lift Equations 289 Introduction 289
B.1	
B.2	Minimum Casing Pressure 289
B.3	Maximum Casing Pressure 291
B.4	Summary 291
	Reference 292
Appendix	C: Gas Fundamentals 293
C.1	Introduction 293
C.2	Phase Diagram 293
C.3	Gas Apparent Molecular Weight and Specific Gravity 293
C.4	Gas Law 295
C.5	Z Factor 296
C.6	Gas Formation Volume Factor 298
C.7	Pressure Increase in Static Column of Gas 299
C.8	Calculate the Pressure Drop in Flowing Dry Gas Well:
	Cullender and Smith Method 300
C.9	Pressure Drop in a Gas Well Producing Liquids 302
	C.9.1 Calculated Result with Dry Gas and Gas
	with Liquids 303
C.10	Gas Well Deliverability Expressions 303
	C.10.1 Backpressure Equation 303
	C.10.2 Darcy Equation 305
	References 307
Index 30	9

14.4 Tubing/Annulus Switching Control 279

PREFACE

Most gas well streams contain water or condensate. As the well pressure and production rate decline, liquids begin to accumulate in the tubing or flow path. *Gas Well Deliquification* contains methods of predicting and analyzing this situation. Also presented are many proven methods that are used in the oil and gas industry to eliminate or reduce the effects of liquid loading so that gas well production can proceed with minimal interference. This collection of information should be helpful to many gas well producers.

James Lea Henry Nickens Michael Wells

INTRODUCTION

1.1 INTRODUCTION

Liquid loading of a gas well is the inability of the produced gas to remove the produced liquids from the wellbore. Under this condition, produced liquids will accumulate in the wellbore leading to reduced production and shortening of the time until when the well will no longer produce.

This book deals with the recognition and operation of gas wells experiencing liquid loading. It presents materials on methods and tools to enable you to diagnose liquid loading problems and indicates how to operate your well more efficiently by reducing the detrimental effects of liquid loading on gas production.

This book will serve as a primer to introduce most of the possible and most frequently used methods that can help produce gas wells when liquids begin to become a problem. Liquid loading can be a problem in both high rate and low rate wells, depending on the tubular sizes, the surface pressure, and the amount of liquids being produced with the gas. In this book you will learn:

- How to recognize liquid loading when it occurs
- How to model gas well liquid loading
- How to design your well to minimize liquid loading effects
- What tools are available to assist you in the design and analysis of gas wells for liquid loading problems
- The best methods of minimizing the effects of liquids in lower velocity gas wells and the advantages and disadvantages of these methods
- How and why to apply various artificial lift methods for liquid removal

 What should be considered when selecting a lift method for liquid removal

1.2 MULTIPHASE FLOW IN A GAS WELL

To understand the effects of liquids in a gas well, we must understand how the liquid and gas phases interact under flowing conditions.

Multiphase flow in a vertical conduit is usually represented by four basic flow regimes as shown in Figure 1-1. A flow regime is determined by the velocity of the gas and liquid phases and the relative amounts of gas and liquid at any given point in the flowstream.

One or more of these regimes will be present at any given time in a well's history.

• **Bubble Flow**—The tubing is almost completely filled with liquid. Free gas is present as small bubbles, rising in the liquid. Liquid contacts the wall surface, and the bubbles serve only to reduce the density.

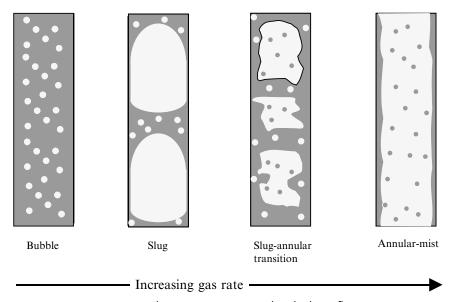


Figure 1-1. Flow regimes in vertical multiphase flow.

Introduction 3

• Slug Flow—Gas bubbles expand as they rise and coalesce into larger bubbles and then slugs. Liquid phase is still the continuous phase. The liquid film around the slugs may fall downward. Both gas and liquid significantly affect the pressure gradient.

- Slug-Annular Transition—The flow changes from continuous liquid to continuous gas phase. Some liquid may be entrained as droplets in the gas. Although gas dominates the pressure gradient, liquid effects are still significant.
- Annular-Mist Flow—Gas phase is continuous, and most of liquid is entrained in the gas as a mist. Although the pipe wall is coated with a thin film of liquid, the pressure gradient is determined predominately from the gas flow.

A gas well may go through any or all of these flow regimes during its lifetime. Figure 1-2 shows the progression of a typical gas well from initial production to end of life. In this illustration, it is assumed that the tubing end does not extend to the mid-perforations so that there is a section of casing from the tubing end to mid-perforations.

The well may initially have a high gas rate so that the flow regime is in mist flow in the tubing; however, it may be in bubble, transition, or slug flow below the tubing end to the mid-perforations. As time increases and

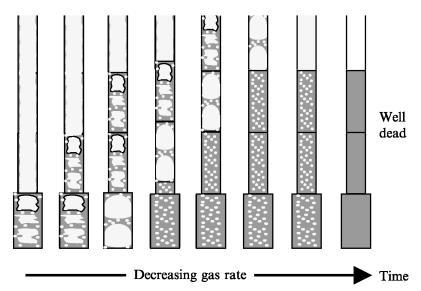


Figure 1-2. Life history of a gas well.

production declines, the flow regimes from the perforations to surface will change as the gas velocity decreases. Liquid production may also increase as the gas production declines. Flow at surface will remain in mist flow until the conditions change sufficiently at the surface so that the flow exhibits transition flow. At this point, the well production will become somewhat erratic, progressing to slug flow as the gas rate continues to decline. This transition will often be accompanied by a marked increase in the decline rate. The flow regime further downhole may be in bubble or slug flow, even though the surface production is in stable mist flow.

Eventually, the unstable slug flow at surface will transition to a stable, fairly steady production rate again as the gas rate declines further. This event occurs when the gas rate is too low to carry liquids to surface and simply bubbles up through a stagnant liquid column.

If corrective action is not taken, the well will continue to decline and will eventually log off. It is also possible that the well may continue to flow for a long period in a loaded condition and that gas produces up through liquids with no liquids rising to the surface.

1.3 WHAT IS LIQUID LOADING?

When gas flows to surface, the gas carries the liquids to the surface if the gas velocity is high enough. A high gas velocity results in a mist flow pattern in which the liquids are finely dispersed in the gas. This results in a low percentage by volume of liquids being present in the tubing (i.e., low liquid "holdup") or production conduit, resulting in a low pressure drop caused by the gravity component of the flowing fluids.

According to the Interstate Oil and Gas Compact Commission, in 2000, 411,793 stripper oil wells in the United States produced an average of 2.16 bpd and 223,707 stripper gas wells produced an average of 15.4 Mscf/D. For the lower-producing gas wells operating on the edge of profitability, optimization and reduction of liquid loading can mean the difference between production and shutting the well in. Liquid loading in gas wells is not limited, however, to the low rate producers; gas wells with large tubulars and/or high surface pressure can suffer from liquid loading even at high rates.

A well flowing at a high gas velocity can have a high pressure drop caused by friction; however, for higher gas rates, the pressure drop caused by accumulated liquids in the conduit is relatively low. This subject is discussed in greater detail later in the book.

Introduction 5

As the velocity of the gas in the production conduit drops with time, the velocity of the liquids carried by the gas declines even faster. As a result, flow patterns of liquids on the walls of the conduit, liquid slugs forming in the conduit, and eventually liquids accumulating in the bottom of the well occur; all of which increase the percentage of liquids in the conduit while the well is flowing. The presence of more liquids accumulating in the production conduit while the well is flowing can either slow production or stop gas production altogether.

Few gas wells produce completely dry gas. Under some conditions, gas wells will produce liquids directly into the wellbore. Both hydrocarbons (condensate) and water may condense from the gas stream as the temperature and pressure change during travel to the surface. In some cases, fluids may come into the wellbore as a result of coning water from an underlying zone or from other sources.

Most of the methods used to remove liquids from gas wells do not depend on the source of the liquids. However, if a remediation method is considered that addresses condensation only, then it must be determined that this is indeed the source of the liquid loading. If not, the remediation will be unsuccessful.

1.4 PROBLEMS CAUSED BY LIQUID LOADING

Liquid loading can lead to erratic, slugging flow and to decreased production from the well. The well may eventually die if the liquids are not removed continuously, or the well may produce at a lower rate than possible.

If the gas rate is high enough to continually produce most or all of the liquids, the wellbore formation pressure and production rate will reach a stable equilibrium operating point. The well will produce at a rate that can be predicted by the reservoir inflow performance relationship (IPR) curve (see Chapter 4).

If the gas rate is too low, the tubing pressure gradient becomes larger because of the liquid accumulation resulting in increased pressure on the formation. As the backpressure on the formation increases, the produced rate from the reservoir decreases and may drop below the so-called "gas critical rate" required to continuously remove the liquid. More liquids will accumulate in the wellbore, and the increased bottomhole pressure will reduce production or may kill the well.

Late in the life of a well, liquid may stand over the perforations with the gas bubbling through the liquid to the surface. The gas is producing at a low but steady rate, and no liquids may be coming to the surface. If this was observed without any knowledge of past well history, one might assume that the well is only a low gas producer, not liquid loaded.

All gas wells that produce liquids—whether in high or low permeability formations—will eventually experience liquid loading with reservoir depletion. Even wells with very high gas-liquid ratios (GLR) and small liquid rates can load up if the gas velocity is low. This condition is typical of very tight formation (low permeability) gas wells that produce at low gas rates and have low gas velocities in the tubing. Some wells may be completed and produce a considerable gas rate through large tubulars, but may be liquid loaded from the first day of production. Lea and Tighe¹ and Libson and Henry² provide an introduction to loading and some discussion of field problems and solutions.

1.5 DELIQUEFYING TECHNIQUES

The following list³ (modified) introduces some of the possible methods to deliquefy gas wells that are discussed here. These methods may be used singly or in combination. This list is based roughly on the static reservoir pressure.

Each of these methods is discussed in some detail. This list is not presented as being 100% complete. Special methods, such as using a pumping system to inject water below a packer to allow gas to flow up the casing-tubing annulus, are covered in the chapters on de-watering using beam and ESP pumping systems. Depth considerations and certain economic considerations also are not detailed.

The method that is most economic for the longest period of operation is the optimum method. The criteria for selecting the optimum method are: methods in similar fields that are used successfully, vendor equipment availability, reliability of equipment, manpower required to operate the equipment, and lifting capacity.

- Reservoir Pressure >1500 psi
 - Evaluate best natural flow of the well
 - Use Nodal Analysis to evaluate the tubing size for friction and future loading effects
 - Consider possible coiled tubing use